

AMENDMENT UNDER 37 C.F.R. §1.111

In the specification:

Please change the paragraph beginning on page 11, line 1 to read as follows:

The amount of surfactant, used in the emulsions of the present invention can be as high as about 20 wt % but is preferably between about 5 and about 15 wt % with a wt % of about 8 to about 12 being more preferred. Amounts much over about 15 wt % are generally not needed, however, minor amounts below about 3 wt % tend to be inadequate. Examples of suitable surfactants include Ingepal's CO series such as Ingepal CO-630, and Ingepal CO-710; nonylphenyl and ethoxylated alcohols such as Tergitol 15-S-9 and Tergitol 15-S-12.

Please change the paragraph beginning on page 11, line 17 to read as follows:

The emulsion can also contain other ingredients such as bleaching agents or whitening agents such as sodium metabisulfite. Although the bleaching agent or whitening agent is generally not needed, minor amounts often do decrease the color. The concentration of the bleaching agent may be as high as about 1 wt %, but is preferably about 0.1 to about 0.5 wt %, and more preferably about 0.2 to about 0.4 wt %.

Please change the paragraph beginning on page 13, line 5 to read as follows:

The thermally degraded polypropylenes (ACX1089, ACX1172, or blends thereof) from Allied _ Signal, Inc., were melted at a temperature of 190° C., sparged with nitrogen gas, and agitated. The reactant monomer, maleic anhydride, and catalyst DTBP, were fed into the reaction mass at very precise rates over a period of 1 hour with the catalyst feed rate exceeding the maleic anhydride feed rate by 25%. The products were sparged with nitrogen

to remove by-products and discharged. The resultant products 597 and 1221 Waxes had a saponification number from 30 to 90 mg KOH/g depending on the amount of maleic anhydride charged, grafting efficiency typically 70-75%, viscosity 300 to 900 cps at 190° C., and Gardner color 8 or less. The MW of the products were typically less than 25,000 and Mw/Mn less than 5.

Please change Table 1, beginning on page 14, line 2 to read as follows:

Table 1. Emulsion Clarity Data

<u>Run</u>	<u>Sap</u> <u>No:</u> <u>(d)</u> <u>gm</u> <u>KOH</u> <u>(a)</u>	<u>gm</u> <u>Surf</u> <u>(g)</u> <u>(d)</u> <u>(b)</u>	<u>Agitation</u> <u>(RPM)</u>	<u>Solids</u> <u>(g)</u> <u>(%)</u>	<u>pH</u>	<u>Klett</u> <u>(c,d)</u>	<u>%T</u> <u>(d)</u>
Wax 597	25	60	300	41	10	28	55
					8.9	27	52.4
Wax 1221(a)	11	60	300	40	8.7	55	32.5
E43 (b)	19	50	200	40	9.5	510	0.1
E43 (c)	25	60	300	40	12.8	380	0

Please change the paragraph beginning on page 15, line 15 to read as follows:

In this example co-emulsions of Wax 597 with a high molecular weight, low saponification number (Mw 50,000, SN about 20 mg KOH/g) maleated Polypropylene which was internally synthesized (commercial Montell feedstock) were made as previously described in Example 1. Figure 1 shows the Klett/clarity of the emulsion as a function of the Mw amount of the typically unemulsible polypropylene in the co-emulsion. Therefore, the